Model for Calculating the Viscosity of Aqueous Solutions, Marc Laliberté,* J. Chem. Eng. Data 2007, 52, 321–335.

Page 326. A parenthesis was misplaced in eq 12:

$$(\eta_i/\text{mPa}\cdot\text{s}) = \frac{e^{[(v_1(1-w_w)^{v_2}+v_3)/(v_4(t)^\circ\text{C})+1)]}}{v_5(1-w_w)^{v_6}+1}$$
(12)

where η_i is the solute viscosity; w_w is the mass fraction of water, and v_1 to v_6 are dimensionless empirical constants.

Equation 13 needs to be corrected accordingly:

$$\ln(\eta_{i}/\mathrm{mPa} \cdot \mathrm{s}) = \frac{v_{1}(1 - w_{w})^{\nu_{2}} + v_{3}}{(v_{4}t/^{\circ}\mathrm{C} + 1)\ln\{v_{5}(1 - w_{w})^{\nu_{6}} + 1\}}$$
(13)

The spreadsheets attached as Supporting Information to the review have not been changed, as the formulas in Excel were correct.

For NaClO₃ and MgSO₄, an older correlation for calculating the viscosity of water was used. This has a slight impact on the calculation of v_1 to v_6 as this older correlation was less accurate.

For the components below, the wrong molecular weight was used to convert mole-based concentration (mole fraction, molarity, or molality) to mass fractions. The overall error in calculating v_1 to v_6 is variable and depends on how inaccurate the molecular weight was, on how many data points were mole-based, and on their value (the error is lower when the concentration is lower). For Na₂CO₃, the K₂CO₃ MW was used. The MW of CaCl₂ was used for Ca(NO₃)₂, Cd(NO₃)₂, Cu(NO₃)₂, HCH₃COO, KBr, KCH₃CO₂, KH₂PO₄, KI, Li(NO₃)₂, Mg(NO₃)₂, Na₂S₂O₃, NH₃, Pb(NO₃)₂, Sr(NO₃)₂, and sucrose.

Finally, the density and viscosity data for $Ni(NO_3)_2$ that were ready for publication but were overlooked have been added.

With all these changes, the average difference between the calculated and experimental viscosities for all the available data is 0.03 %. (The average of all experimental viscosities of solution of one solute in water is 2.2 mPa·s, and the average difference between the experimental and calculated viscosity is 0.0006 mPa·s.) The standard deviation of this difference is 3.5 % of the average viscosity (down from 3.7 %).

Table 2 has been updated with these changes. Because of the length of the table, it is not possible to reprint the data for the components where no change has occurred. The reader is referred to either the original publication or to the file _PropertiesAqueousSolution.xls in the Supporting Information for these components.

These changes have reduced the error when predicting the viscosity for mixtures. The two worse mixtures were the LiCl and LiNO₃ system where the standard deviation $s_{\delta_{\eta}}$ is unchanged at 25 % and the Ca(NO₃)₂ and NaCl system where it went down to 4.3 % from 55 %. Table 5 is not reprinted because of space constraints, and the reader is again referred to the Supporting Information.

Supporting Information Available:

Calculation spreadsheets for all the solutions presented in the original review. This material is available free of charge via the Internet at http://pubs.acs.org.

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name	Ca(NO ₃) ₂	Cd(NO ₃) ₂	Cu(NO ₃) ₂	HCH ₃ CO ₂	KBr	KCH ₃ CO ₂	
v_1	69.623	7.7484	10.728	-1.4323	348.32	6.5787	
v_2	4.9340	2.1518	1.7784	9.9878	-0.00030253	2.8228	
v_3	3.4578	2.5049	2.1116	3.5600	-349.15	3.7025	
v_4	0.010566	0.0096163	0.0083713	0.015191	-0.0042580	0.013558	
v_5	1883.8	0.86015	-3.4975	3.1883	-1.1044	0.13910	
v_6	12.100	-0.068299	2.0697	0.43029	0.76315	-0.64166	
min t/°C	-10	15	25	15	0	15	
max t/°C	100	55	25	55	95	55	
$\max w_i$	0.603	0.542	0.458	1	0.462	0.595	
average viscosity	-0.15	0.01	0.02	-0.23	0.00	0.09	
residual $\delta_{\eta}/\%$							
SD of viscosity	1.1	0.20	0.26	1.4	1.1	0.79	
residual $s_{\delta_n}/\%$							
no. of points in	72	84	10	238	347	126	
correlation							
no. of inconsistent	2	7	0	0	6	0	
points							
references	3, 13,	63, 77, ^{<i>a</i>}	63, <i>^a</i> 74,	34, 57,	20, 43,	66, 124,	
	78, 237,	125, 260,	106	66, 98,	83, 94,	162	
	241.286	261		99, 124,	95, 118,		
	,			161, 162	125, 135,		
					137, 164		
					179 183		
					196, 209		
					228 250		
					220, 230,		
					255, 205,		
		VI	LINO	$M_{\alpha}(NO)$	204, 275 Maso	No CO	
name	KΠ2PO4 40.178	2 0959	LINO3 15.057	$\frac{1}{72}$ 708	Mg504	Na2CO3	
<i>v</i> ₁	49.178	2.9636	1 4 2 0 6	12.198	12.209	21.///	
v_2	2.0055	2.3770	1.4390	4.5110	2.2238	6 4262	
<i>V</i> ₃	1.2471	0.49977	1.3431	4.1044	0.0037	0.4303	
v_4	0.012550	1 7020	0.0078574	0.012550	0.0079004	0.013223 6.0002E 20	
<i>U</i> ₅	-0.07910	0.0016505	125.55	12347	5540.1	-0.9095ET20	
v_6	17.690	-0.0010303	5.5155	20.972	0.1504	42.050	
$\lim_{t \to \infty} t/^{\circ}C$	19.95	5 05	110	23	150	20	
max <i>u</i> C	0.222	95	0.671	0.72	0.202	90	
$max w_i$	0.232	-0.01	-0.04	-0.02	0.505	0.306	
average viscosity	0.05	-0.01	-0.04	-0.02	0.01	0.52	
SD of viscosity	0.2	1.2	27	2.0	0.00	2.2	
sD of viscosity	9.2	1.2	2.1	2.0	0.90	2.5	
residual $s_{\delta_{\eta}}$ /%	60	245	104	56	190	51	
no. of points in	00	245	104	50	180	51	
correlation	0	0	25	0	12	0	
no. of inconsistent	0	0	23	0	15	0	
references	A7 a 50	12 62	14 20	62 115	16 17	52 112	
Tererences	47, 50,	43, 02,	14, 50,	128 241	10, 17,	116 168	
	170, 164	94, 142, 164, 170	31, 241, 202, 200	130, 241, 256, 262	43, 44,	170, 206	
		104, 179,	293, 300	200, 203,	07, 79,	179, 200	
		165, 190,		290	60, 115, 125, 124		
		223, 228,			125, 154,		
		250, 255,			140, 150,		
		254			1/7, 179,		
					182, 206,		
					209, 228,		
					248, 263		
name	$Na_2S_2O_3$	NaClO ₃	NH ₃	$N_1(NO_3)_2$	$Pb(NO_3)_2$	$Sr(NO_3)_2$	sucrose
v_1	18.291	20.952	214.09	23.288	3.9904	12.449	16.239
v_2	2.1091	0.32364	8.0241	2.14217	1.3862	1.6546	1.4693
v_3	2.3485	-6.1134	6.6265	1.9926	1.3591	1.0765	3.2849
v_4	0.016497	0.0019919	0.0057943	0.0083713	0.028370	0.0083713	0.010285
v_5	6.0523E+12	24387	255.27	52.492	62.501	7.3912	33.939
v_6	68.515	3.0662	0.24309	3.7236	5.3410	2.0697	2.2817
min t/C	20	25	20	25	25	25	15
max t/°C	50	55 0.592	40	25	5U 0.275	25	55 0.507
$\max w_i$	0.658	0.583	0.340	0.422	0.375	0.388	0.507
average viscosity	0.10	0.11	-0.08	-0.01	0.02	0.01	-0.20
residual $\partial_{\eta}/\%$	4.2	5.0	1.4	0.10	5 4	0.07	0.71
SD of viscosity	4.3	5.9	1.4	0.19	5.4	0.07	0.71
residual $s_{\delta_{\eta}}$ /%				10		-	
no. of points in	26	34	25	12	14	7	81
correlation	0	0	0	0	<u>_</u>	0	0
no. of inconsistent	0	0	0	0	0	0	0
points	100 100	27 12	24.24	<i>(</i> 2)	10 - 52	(2) 172	101 10-
references	139, 193,	37, 43,	24, 84,	63	43, 63,	63, 172,	124, 183,
	209, 260	209, 240	163, 209,		115, 228	263	249
			231, ^a 243 ^a				

Table 2.	Results	for	Solutions	of	One	Solute	in	Water ^a	

^a For references marked with this symbol, see the Supporting Information for additional notes or qualifiers.